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# Getting More From Your Intelligent Pig Inspection

by

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Penspen Integrity

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Aberdeen  
14 – Nov 2007



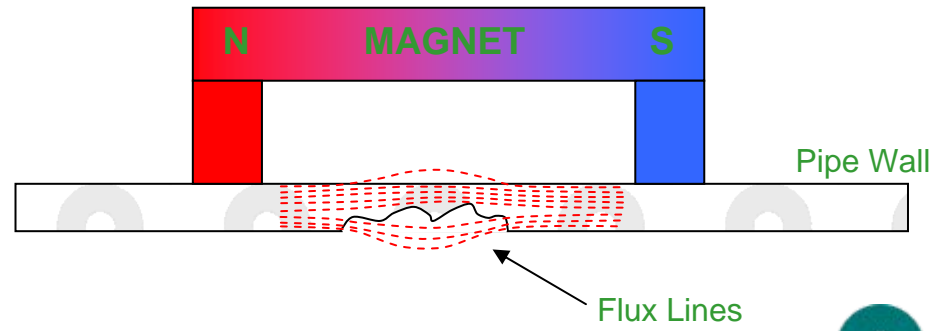
# The Problem

- Intelligent pigs are widely used
- Large quantities of data are collected
- Defects are generally reported in a simple spreadsheet format.
- Simple clustering and defect sizing leads to safe conservative assessments

# Outline

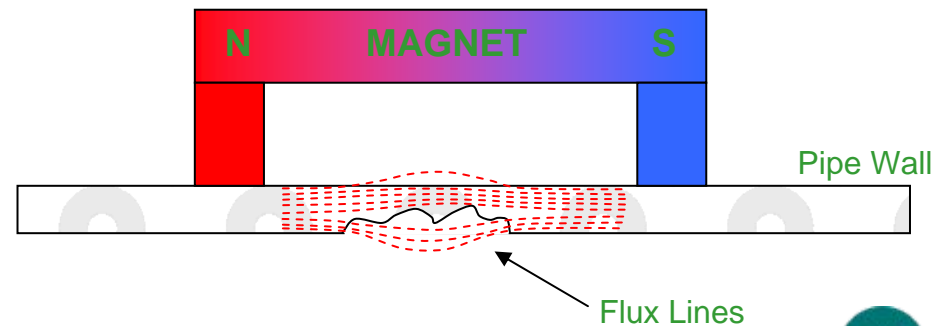
- Inspection Technology
  - MFL
  - UT
- Defect Sizing
- Defect Assessment
- ‘Complex Shape’ Assessment
- Case Study

# MFL Inspection

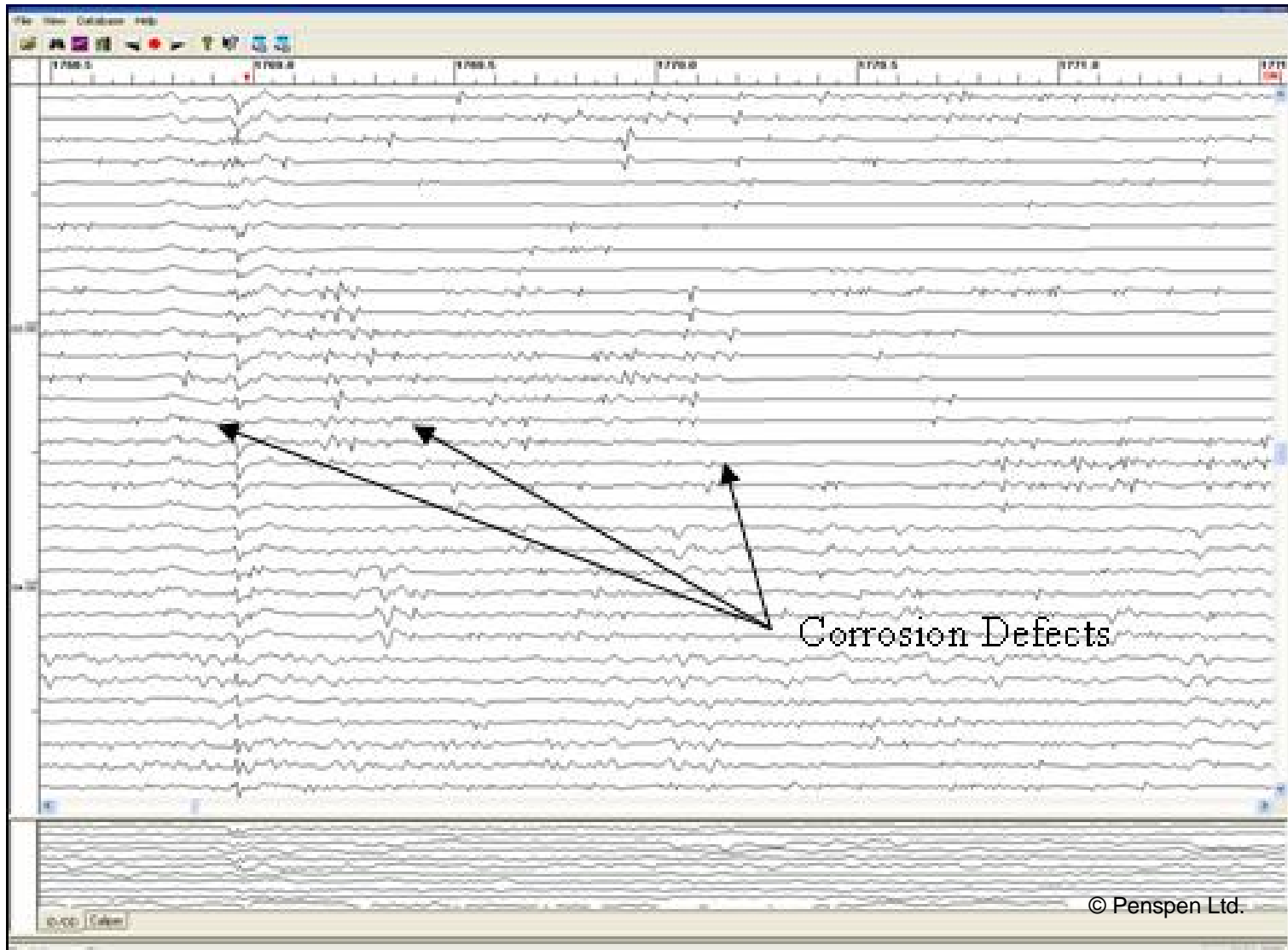


# MFL Defect Sizing

- Relative measurement
- Depth
  - Signal amplitude
  - Number of sensors affected

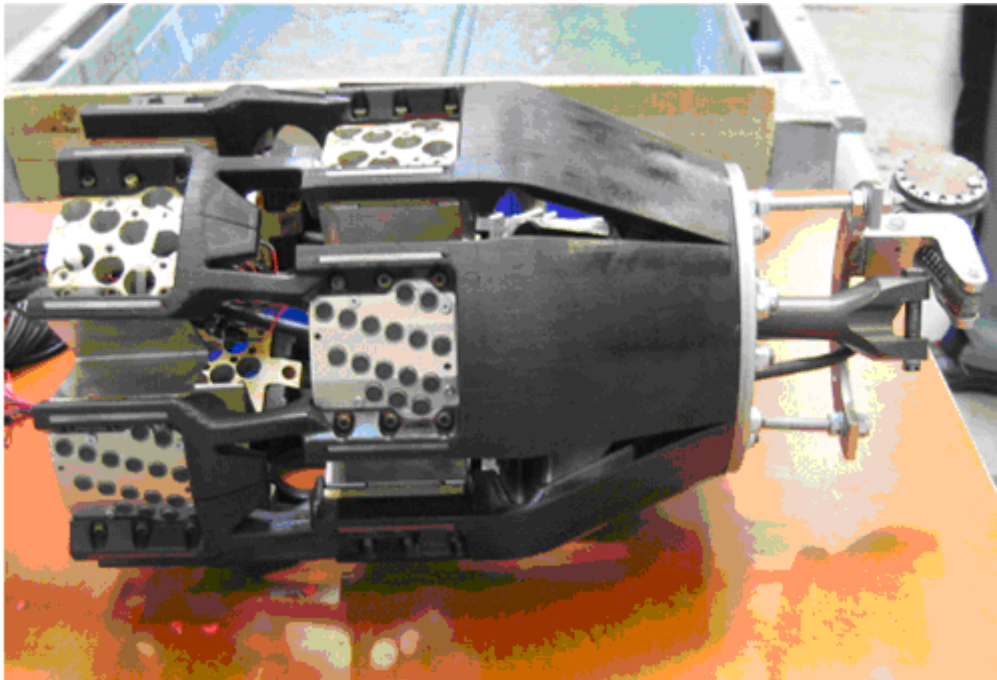
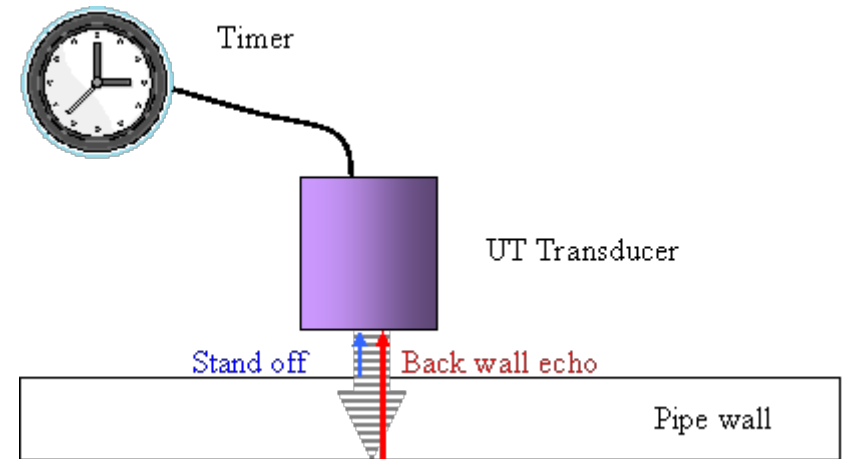


# MFL Data



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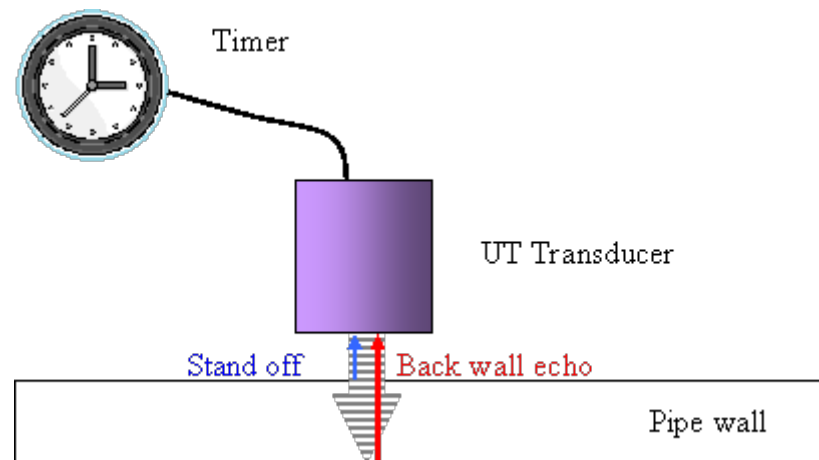
# UT Inspection



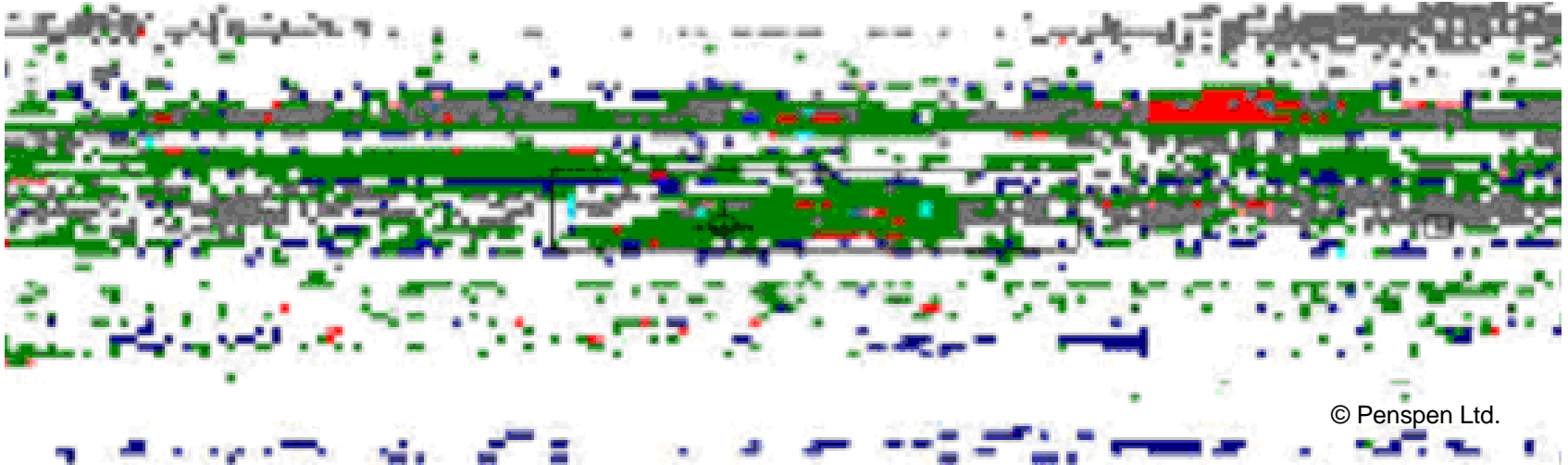


# UT Defect Sizing

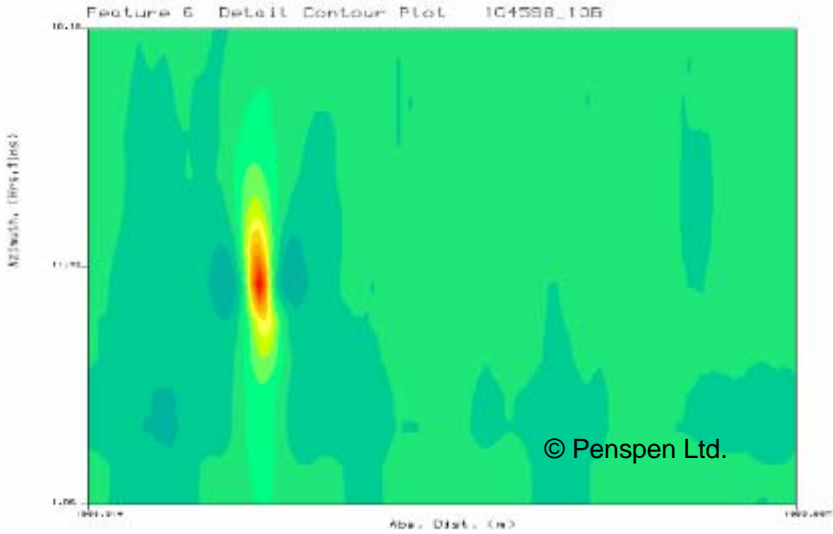
- Absolute Depth/Wall Thickness
  - Time difference between echo signals



# UT Data



# Individual Defects

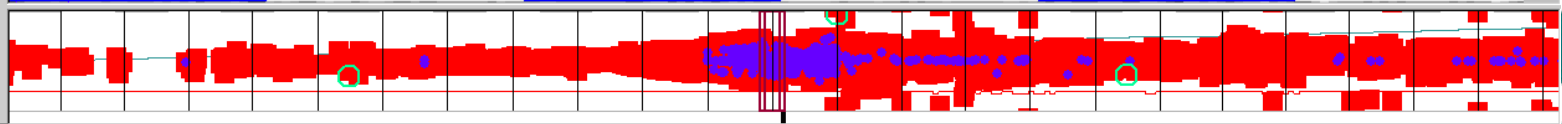
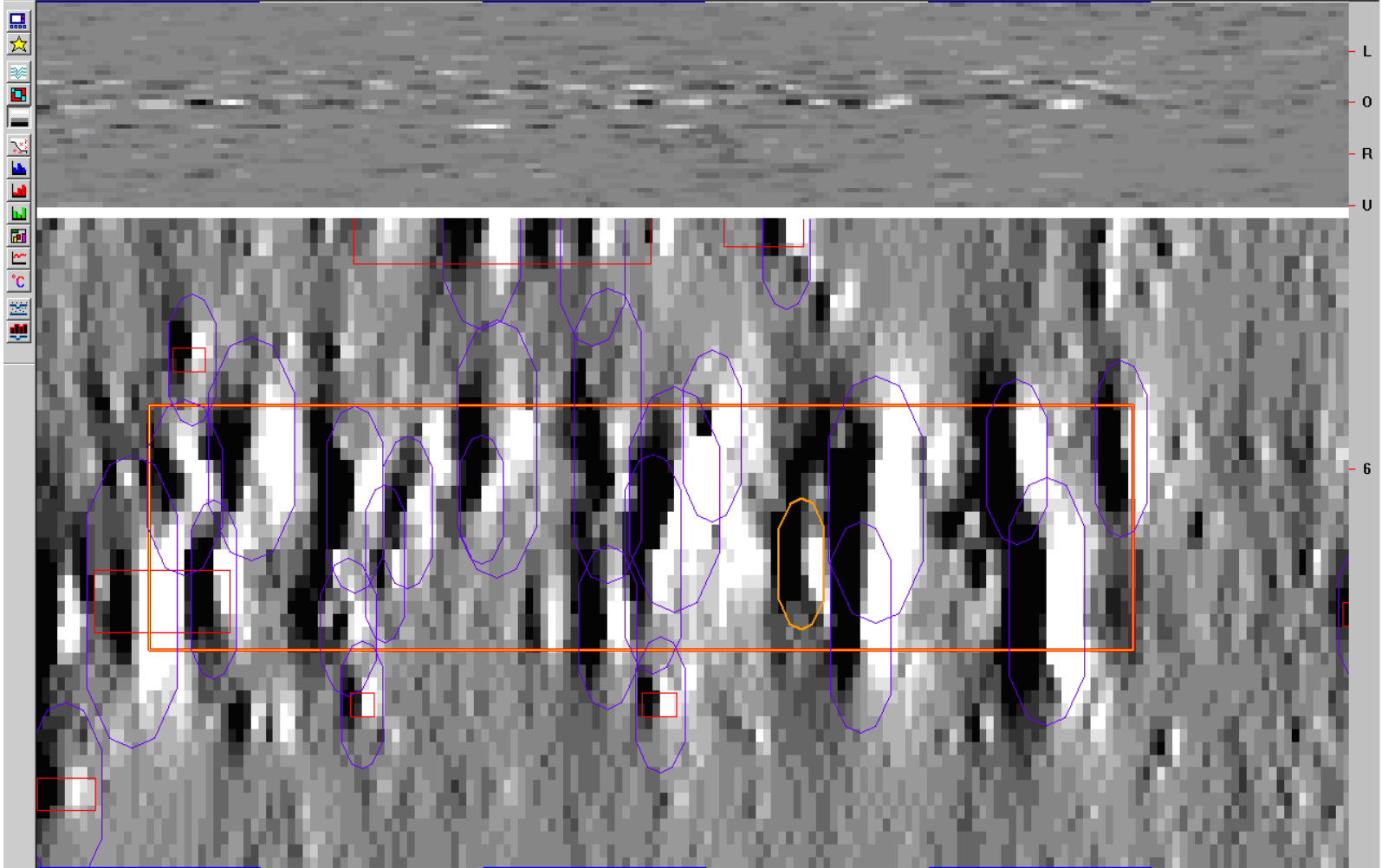


# Multiple Defects?

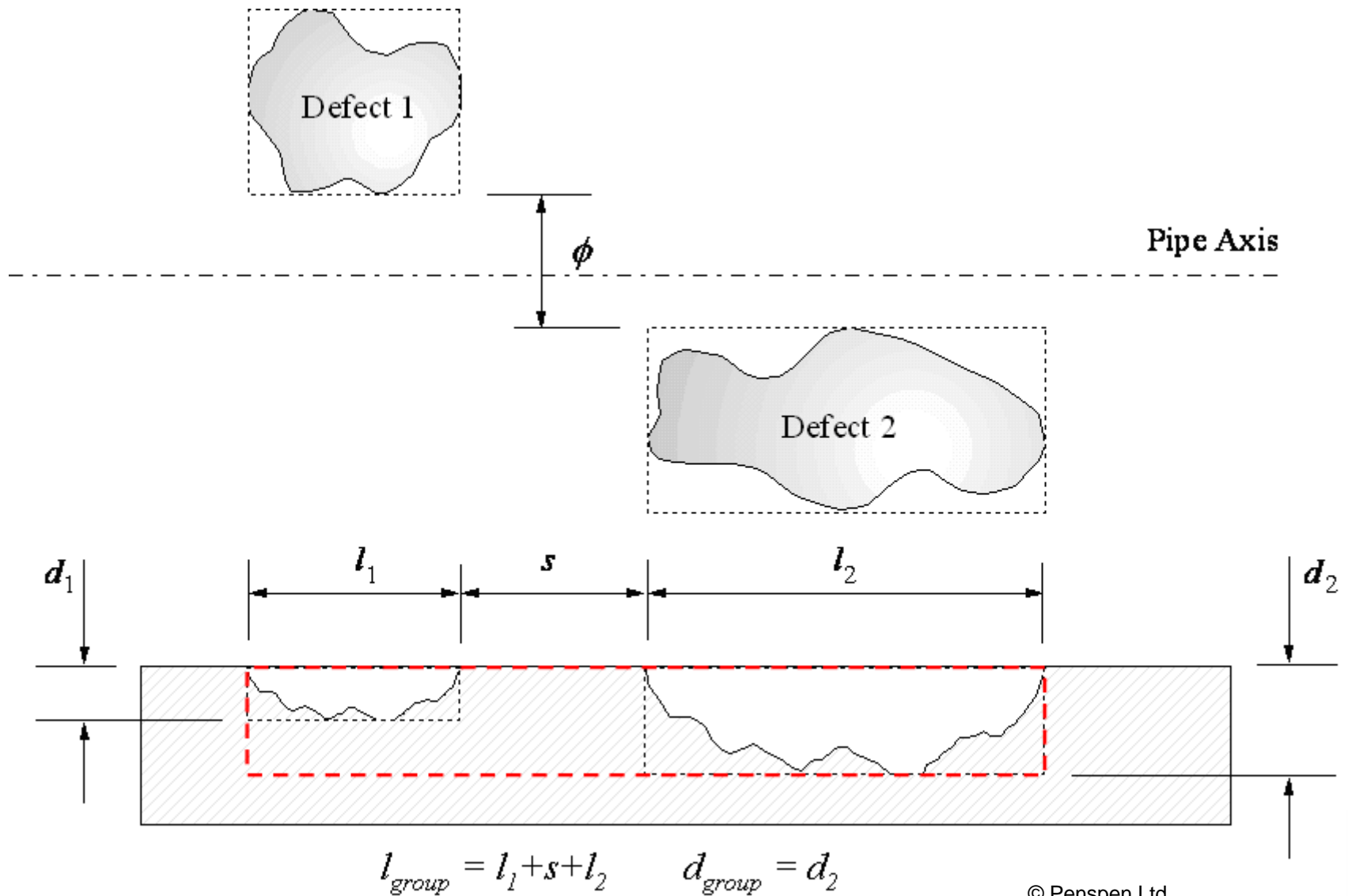


26% (13.5 len x 14.0 wid)

Metal Loss

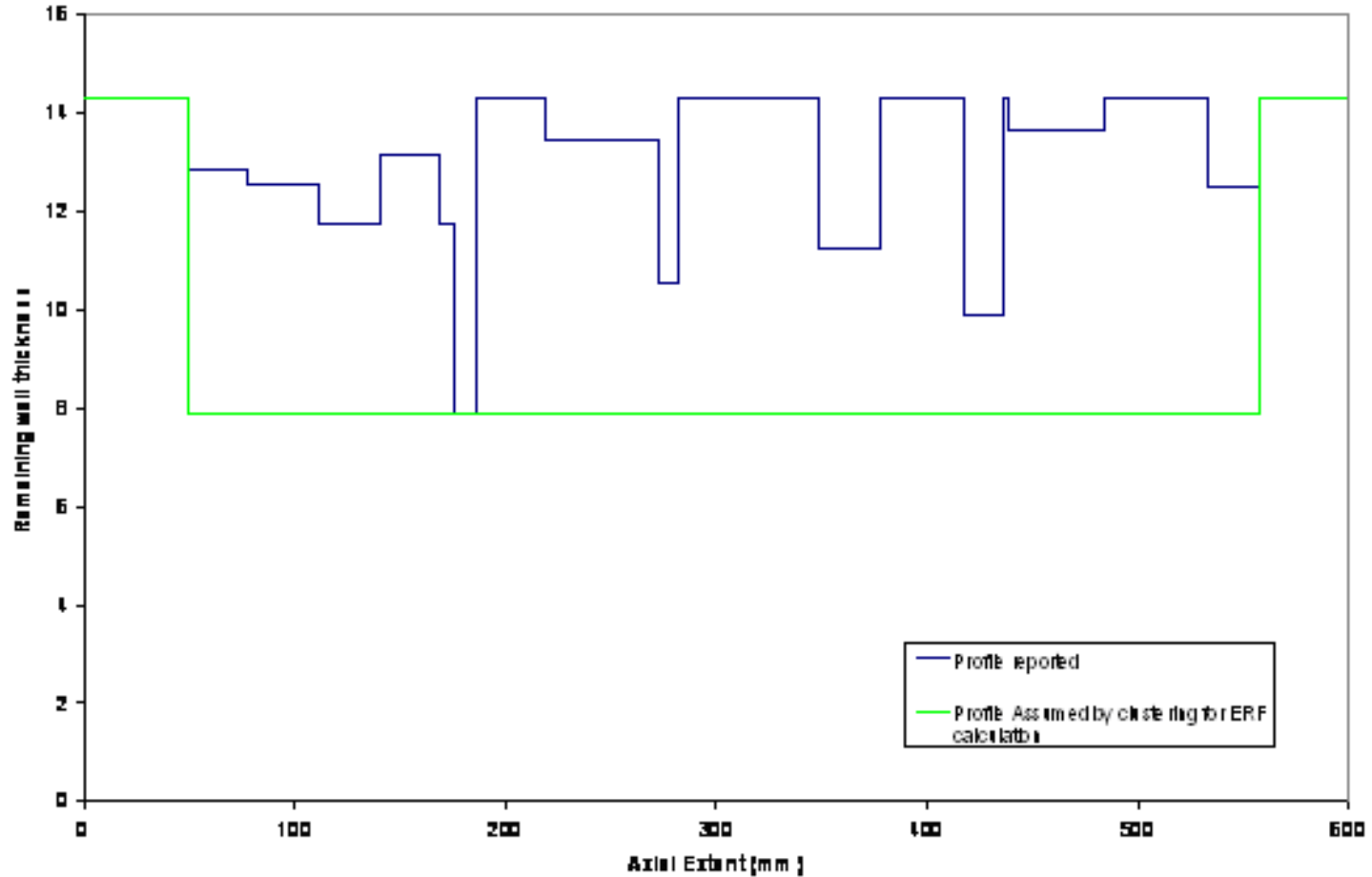


# Clustering



Upstream Girth Weld	Relative Distance (metres)	Absolute Distance (metres)	Comment	Peak Depth (%wt)	Length (mm)	ERF	Orientation (hrs:mins)
30	10.6	19.6					
40	9.7	29.4					
50	0.7	30.1	NWT 7.80/9.53MM				
60	3.0	33.1	NWT 9.53/7.80MM				
	0.2	33.3	*EXT ML	21%	79	0.260	02:15
63	0.2	33.3					
68	5.3	38.7		40%	694	0.406	05:45
	0.0	38.7	*EXT ML				
70	0.7	39.4	NWT 7.80/9.53MM				
	0.1	39.6	EXT ML	26%	19	0.245	05:00
80	3.0	42.5	NWT 9.53/7.80MM				
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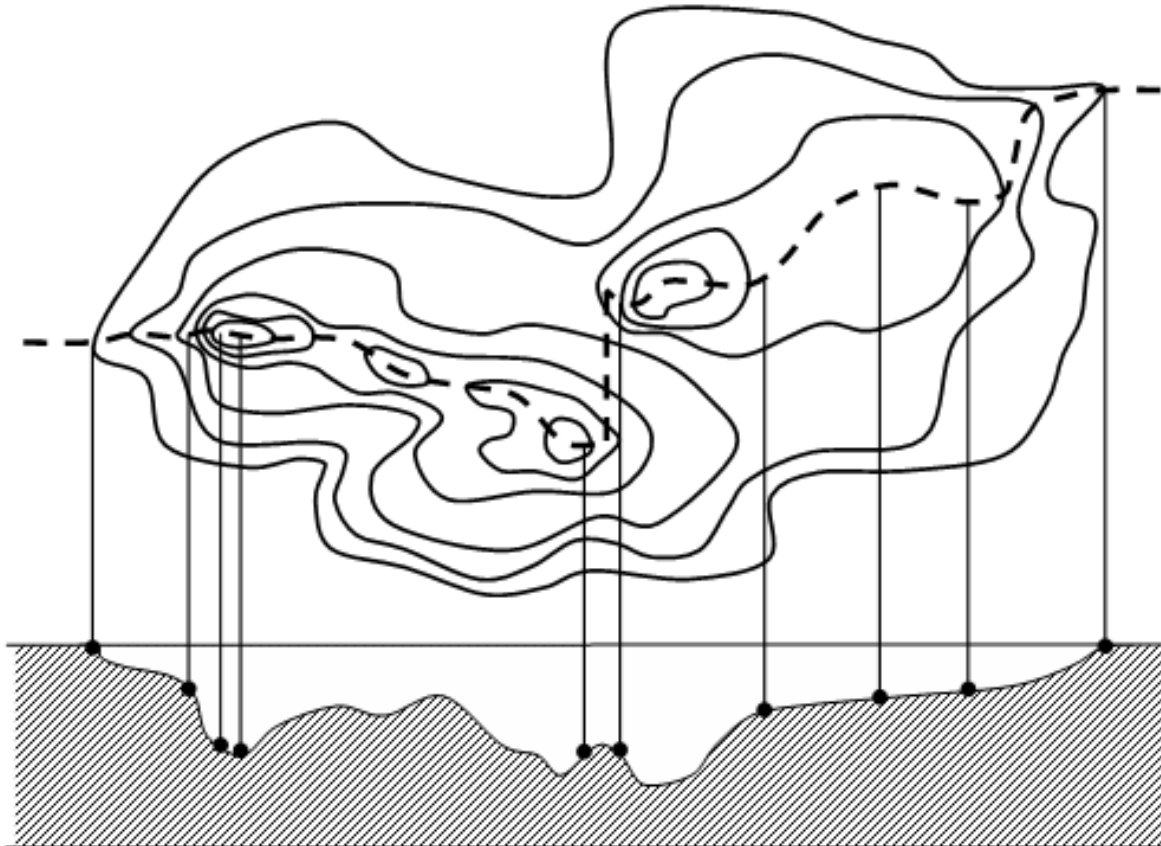
# Cluster





# Evaluation Based on 'Actual' Shape

- RSTRENG – Riverbottom Profile
- DNV RP-F101 Complex Shape Method

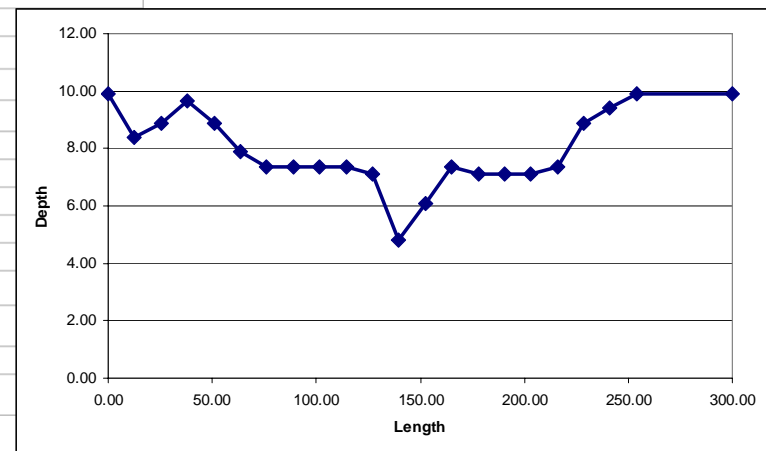


# RSTRENG

20. CORROSION		
20.12 INTERNAL PRESSURE (BURST)		
(RSTRENG)		
KIEFNER, J. F., VIETH, P. H.; <i>A Modified Criterion for Evaluating the Strength of Corroded Pipe</i> , Final Report for Project PR 3-805 to the Pipeline Supervisory Committee of the American Gas Association, Battelle, Ohio, 1989.		
Reference should be made to the Pipeline Defect Assessment Manual		
	symbol, units	value
outside diameter	D, mm	914.4
wall thickness	t, mm	
specified minimum wall thickness	t, mm	9.906
hydrotest pressure	bar	75.0
design pressure	bar	60.0
MAOP	bar	60.0
minimum design temperature	C	
grade (API 5L or equivalent)		X60
SMYS	Nmm <sup>-2</sup>	413.7
SMTS	Nmm <sup>-2</sup>	517.1
maximum corrosion defect depth	d, mm	5.08
	d/t, percent	51.28
maximum corrosion defect length (longitudinal)	2c (L), mm	254.0
<b>predicted failure stress</b>	<b>Nmm<sup>-2</sup></b>	<b>413.63</b>
<b>predicted failure pressure</b>	<b>P<sub>f</sub>, bar</b>	<b>89.62</b>
<b>safe operating pressure</b>	<b>P<sub>sop</sub>, bar</b>	<b>59.99</b>

RUN ANALYSIS

L	d
mm	mm
0.00	1.27
12.70	1.52
25.40	1.02
38.10	0.25
50.80	1.02
63.50	2.03
76.20	2.54
88.90	2.54
101.60	2.54
114.30	2.54
127.00	2.79
139.70	5.08
152.40	3.81
165.10	2.54
177.80	2.79
190.50	2.79
203.20	2.79
215.90	2.54
228.60	1.02
241.30	0.51
254.00	0.00



# DNV RP-F101

PIPELINE DEFECT ASSESSMENT MANUAL		
20. CORROSION		
20.12 INTERNAL PRESSURE (BURST)		
DNV-RP-F101, <i>Corroded Pipelines</i> , Det Norske Veritas, 1999.		
Reference should be made to the Pipeline Defect Assessment Manual		
	symbol, units	value
outside diameter	D, mm	762.0
wall thickness	t, mm	
specified minimum wall thickness	t, mm	22.1
hydrotest pressure	bar	75.0
design pressure	bar	60.0
MAOP	bar	60.0
grade (API 5L or equivalent)		X60
SMYS	Nmm <sup>-2</sup>	413.7
SMTS	Nmm <sup>-2</sup>	517.1
2/3 Charpy V-notch impact energy	J	62.0
maximum corrosion defect depth	d, mm	17.1
	d/t, percent	77.38
maximum corrosion defect length (longitudinal)	2c (L), mm	572.0
'lower bound' predicted failure stress	Nmm <sup>-2</sup>	201.81
'lower bound' predicted failure pressure	P <sub>f</sub> , bar	120.56
safe operating pressure	P <sub>sop</sub> , bar	86.8

**RUN ANALYSIS**

L	d
mm	mm
0.00	0.00
0.00	3.90
0.80	7.39
1.60	8.70
2.40	9.61
3.20	10.30
4.00	10.83
4.80	11.23
5.60	11.53
6.40	11.74
7.20	11.86
8.00	11.90
163.00	11.90
169.20	12.42
175.40	13.41
181.50	14.28
187.70	15.04
193.90	15.67
200.00	16.19
206.20	16.59
212.30	16.87
218.40	17.04
224.50	17.10
230.60	17.04
236.70	16.87
242.80	16.59
249.00	16.19
255.10	15.67
261.30	15.04
267.50	14.28
273.60	13.41
279.80	12.42
286.00	11.30
292.20	12.42
298.40	13.41
304.50	14.28
310.70	15.04
316.90	15.67
323.00	16.19
329.20	16.59
335.30	16.87
341.40	17.04
347.50	17.10
353.60	17.04
359.70	16.87
365.80	16.59
372.00	16.19
378.10	15.67
384.30	15.04
390.50	14.28
396.60	13.41
402.80	12.42
409.00	11.90
564.00	11.90
564.80	11.86
565.60	11.74
566.40	11.53
567.20	11.23
568.00	10.83
568.80	10.30
569.60	9.61
570.40	8.70
571.20	7.39
572.00	3.90
572.00	0.00

# Example 1

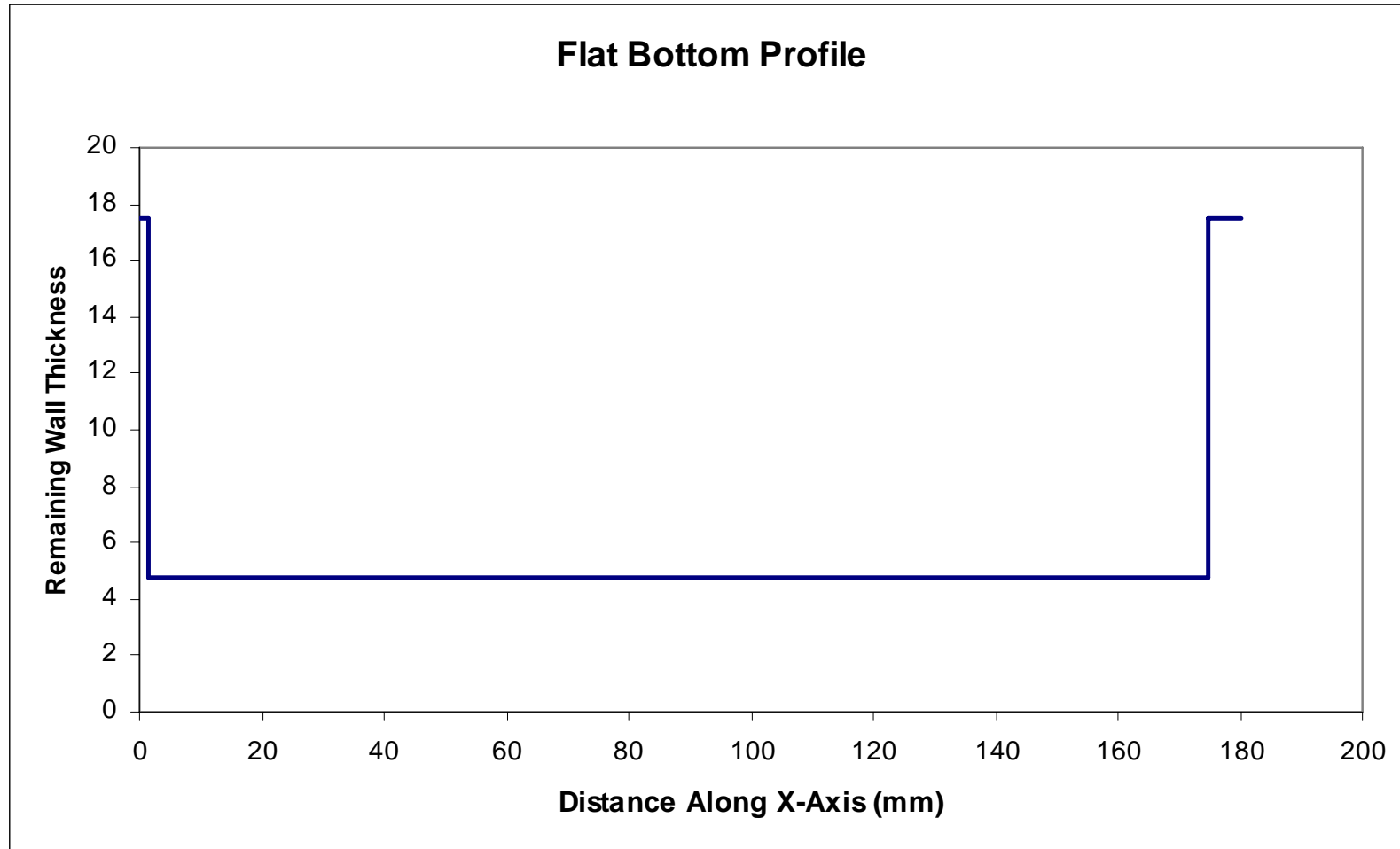
# UT data



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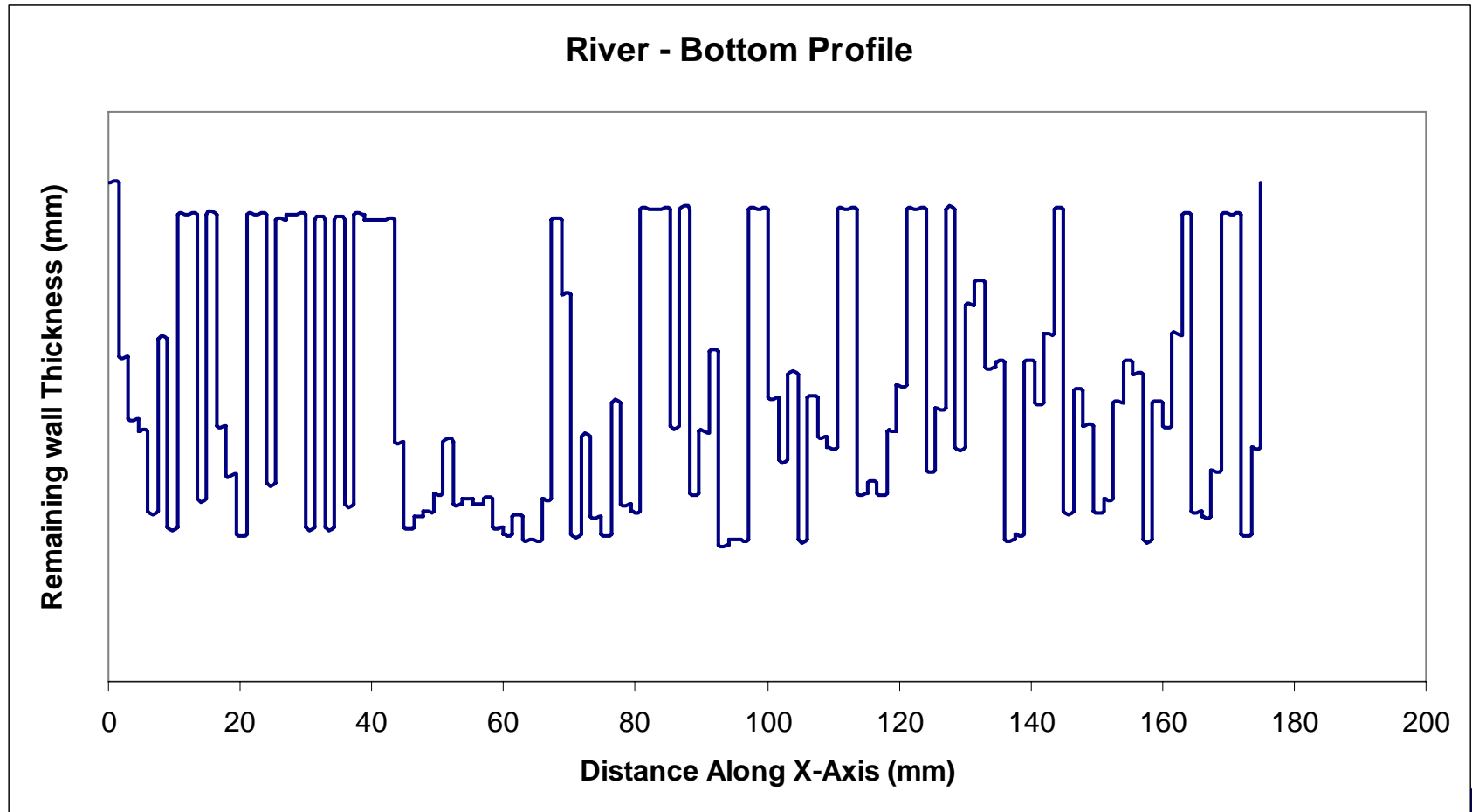
# Rectangular Profile

## Failure Pressure 219 bar



# Riverbottom Profile

## Failure Pressure 305 bar



## Example 2

<b>Assessment</b>	<b>Data</b>	<b>Maximum Reported Depth (%t)</b>	<b>Length (mm)</b>	<b>Defect Profile</b>	<b>Failure Pressure (Bar)</b>
Standard	MFL pig 'Cluster'	63	330	Rectangular	53
Expert	MFL pig 'Boxes'	63	330	'River-Bottom'	113
Expert	External UT	50.5	1760	'River-Bottom'	85



# Inspection/Repair Can be Expensive



# Summary

- Defect profile data gives assessment benefits
- Profile data is collected anyway and so should be supplied in an accessible format with the inspection report.